



## Degradation of decabromodiphenyl ether by nano zero-valent iron immobilized in mesoporous silica microspheres

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### ABSTRACT

The agglomeration of nanoparticles reduces the surface area and reactivity of nano zero-valent iron (NZVI). In this paper, highly dispersive and reactive NZVI immobilized in mesoporous silica microspheres covered with FeOOH was synthesized to form reactive mesoporous silica microspheres (SiO<sub>2</sub>@FeOOH@Fe). The characteristics of SiO<sub>2</sub>@FeOOH@Fe were analyzed by transmission electron microscopy, Fourier transform infrared spectroscopy simultaneous thermal analysis, X-ray photoelectron spectroscopy, and Brunnaer–Emmett–Teller surface area analysis. The mean particle size of the reactive mesoporous silica microspheres was 450 nm, and its specific surface area was 383.477 m<sup>2</sup> g<sup>-1</sup>. The degradation of decabromodiphenyl ether (BDE209) was followed pseudo-first-order kinetics, and the observed reaction rate constant could be improved by increasing the SiO<sub>2</sub>@FeOOH@Fe dosage and by decreasing the initial BDE209 concentration. The stability and longevity of the immobilized Fe nanoparticles were evaluated by repeatedly renewing the BDE209 solution in the reactor. The stable degradation of BDE209 by SiO<sub>2</sub>@FeOOH@Fe was observed within 10 cycles. Agglomeration-resistance and magnetic separation of SiO<sub>2</sub>@FeOOH@Fe were also performed. The improved dispersion of SiO<sub>2</sub>@FeOOH@Fe in solution after one-month storage and its good performance in magnetic separation indicated that SiO<sub>2</sub>@FeOOH@Fe has the potential to be efficiently applied to environmental remediation.

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### 1. Introduction

Polybromodiphenyl ethers (PBDEs), as efficient flame retardants, have been widely used in electronics, chemicals, electrical, textile and other industries [1,2]. Some studies have been confirmed that PBDEs are ubiquitous persistent organic pollutants in the environment as well as in human and animal bodies [3–5]. The presence of PBDEs in the animal body has been found to affect the balance of thyroid and cause neurotoxicity [6]. Therefore, it is necessary to seek for methods, which have high degradation efficiency and can be used in engineering practice.

Recently, using nanoscale elementary metals, metal oxides, and their composites is a promising method of environmental remediation [7–9]. Compared with zero-valent iron (ZVI), nano zero-valent iron (NZVI) has a larger specific surface area and higher reactivity [10]. NZVI is often used for treating contaminants in aqueous solutions because it could effectively degrade many pollutants, such as organic halogenated hydrocarbons [11,12], nitrates [13], heavy metals [14], insecticides [15], and dyes [16]. And it also showed good reactive ability in BDE209 degradation. In 2010, Shih and Tai

[11] reported that the 2.8 mg L<sup>-1</sup> BDE209 can be rapidly removed by NZVI within 40 min in water solution and the efficiency was much better than that of ZVI. Recently, in our lab, the NZVI was prepared from steel pickling waste liquor and used to remove BDE209 in a water/tetrahydrofuran (4/6, v/v) solution [17]. The results showed that 97.92% of 2 mg L<sup>-1</sup> BDE209 was removed within 24 h by 4 g L<sup>-1</sup> NZVI, which was more effective than ZVI under the same conditions.

Aside from its faster reaction rate than ZVI, NZVI can also be directly injected into polluted groundwater and soil, resulting in the immediate degradation of pollutants [18]. However, due to their small size effect and surface effect, NZVI particles are easily aggregated via Van der Waals and magnetic attraction forces, forming particles with diameters ranging from several microns to several millimeters, or even larger in water [19,20]. The agglomeration of these nanoparticles can reduce the surface area and reactivity of NZVI [20,21]. In addition, the poor transport properties of NZVI in aquifers will limit its practical application in the remediation of toxic pollutants in contaminated environments [22].

Two methods are generally adopted to avoid the agglomeration of nanoscale zero-valent iron particles. One is the use of surfactants [23], starches [24], and cellulose [25] to modify the surface of NZVI. By increasing the steric or electrostatic repulsion between particles, nanoscale particles are stabilized and dispersed. The second

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method involves the embed-immobilization technique, wherein NZVI is loaded onto a functional carrier, such as activated carbon [26,27], a nylon membrane [20,28], or a resin [29]. Radical groups and channels in the carriers can obstruct nanoparticles' clustered. Some carriers can even play certain roles during the degradation process. For instance, Choi et al. [26] developed a new strategy wherein nanoscale Fe was loaded onto activated carbon particles to prepare reactive activated carbon. The particles were avoided to be clustered in the process, and the adsorption capacity for lipophilic pollutants was greatly improved. Recently, the emergence of new materials, such as molecular sieve and silica sphere, which can provide potential carriers to solve the problem of NZVI agglomeration has been attracted interest since they can immobilize various nanoparticles for further applications [19,30]. Meanwhile, surface modification of inorganic core with different inorganic shell to form core-shell structures have shown several applications because these particles show some special properties in optics and catalysis by adjusting their chemical composition and structure order recently [31,32]. Since the good thermal and chemical stability, non-toxicity, and biocompatible capacity, silica spheres are widely used in fabricating core-shell for further application [33,34]. For example, Shen et al. [34] prepared and demonstrated the h-SiO<sub>2</sub>/TiO<sub>2</sub> core/shell microspheres have significant photocatalytic activity in degradation of methyl orange in water. Unfortunately, reports on the preparation and application of composite functional materials with NZVI immobilized in mesoporous silica microspheres or other new carriers are limited, let alone using NZVI immobilized onto mesoporous silica spheres to form core-shell structure to remove toxic organic pollutants.

Hence, a new synthesis method was used to prepare reactive mesoporous silica microspheres with a core-shell structure in this study. Transmission electron microscopy (TEM), X-ray photoelectron spectroscopy (XPS) and temperature-programmed reduction (TPR) were applied to analyze and characterize the material. BDE209 was selected as the contaminant to be removed to study the degradation capacity of the new composite material. The longevity and anti-agglomeration capacity of the composites were also tested.

## 2. Experimental

### 2.1. Materials

A standard solution of decabromodiphenyl ether was purchased from Cambridge Isotope Laboratories (CIL, Andover, U.S.) and used to establish the standard curve. Decabromodiphenyl ether (98%, AR grade) was purchased from Aladdin (Shanghai, China) and used as the degradation sample. Ferrous sulfate (FeSO<sub>4</sub>·7H<sub>2</sub>O, >99%), sodium borohydride (NaBH<sub>4</sub> >98%), PEG, and ethanol (EtOH, 99.7%) were supplied by Tianjin Damao Chemical Agent Company (Tianjin, China). Tetraethoxysilane and dodecylamine were purchased from Aladdin (Shanghai, China). Methanol (HPLC grade) was supplied by Tianjin Kermel Chemical Reagents Company.

### 2.2. Synthesis of materials

#### 2.2.1. Preparation of mesoporous silica microspheres

The synthesis of mesoporous silica microspheres was performed according to the method of Miyaka et al. [35]. The main synthesis steps were as follows: About 0.2224 g of dodecylamine was dissolved in EtOH (62.5 vol%) under magnetic stirring in a 50 mL conical flask. Then, 1.16 mL of undiluted liquid tetraethoxysilane were slowly dropped into the solution, which was then stirred for 30 s and allowed to stand for 3 h under room temperature. The products were separated by centrifugation (centrifugation speed,

4000 rpm; time, 10 min) and rinsed with water and EtOH. Afterwards, the products were kept in a vacuum drying chamber for 4 h at 60 °C, heated in a muffle furnace up to 600 °C at a rate of 10 °C min<sup>-1</sup>, and maintained for 4 h to remove the organic template under high temperature calcination. To regenerate the OH<sup>-</sup> groups lost from the surface of SiO<sub>2</sub> during calcination, the silica microspheres were boiled in water for 2 h [36], and then dried in a drying chamber at 60 °C after centrifugation.

#### 2.2.2. Coating the mesoporous silica microspheres with FeOOH

About 0.5 g FeSO<sub>4</sub>·7H<sub>2</sub>O was added to a 50 mL solution containing 0.5 g PEG. The solution was then treated via ultrasonic vibration for 15 min for complete dissociation. About 0.5 g boiled silica spheres was immersed in the solution for 30 min. The pH of the solution as this time was 4.85. Afterwards, the particles were removed and placed in a drying chamber for 3 h at 110 °C. The dried particles were flushed with water and EtOH and then dried in a vacuum drying chamber for 4 h at 60 °C. This produced silica microspheres covered with FeOOH, presented as SiO<sub>2</sub>@FeOOH.

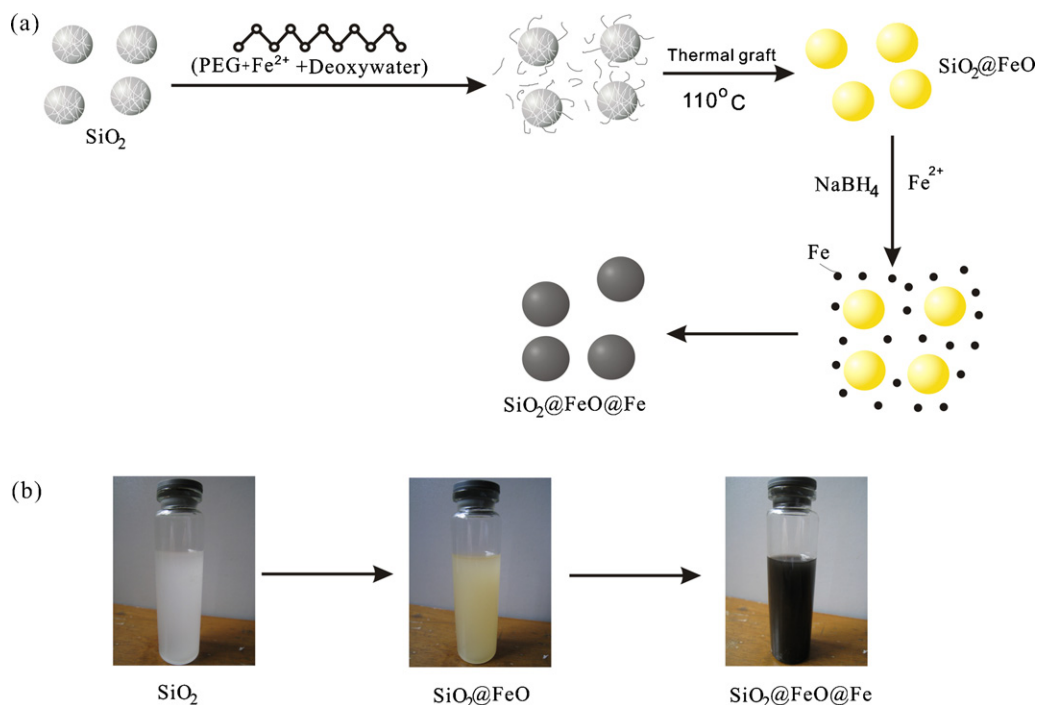
#### 2.2.3. Synthesis of reactive mesoporous silica microspheres

About 0.2 g SiO<sub>2</sub>@FeOOH was put into three flasks, after which 50 mL EtOH (30 vol%) containing 0.2 g FeSO<sub>4</sub>·7H<sub>2</sub>O was added. The solution was stirred well. Then, 20 mL EtOH (30 vol%) with 0.16 g NaBH<sub>4</sub> was added drop-wise while stirring continuously for 10 min. The solution system turned from yellow to black. The products were separated by vacuum filtration and then separately rinsed thrice with water and EtOH. The products were then placed in a drying chamber at 60 °C. Reactive mesoporous silica microspheres, SiO<sub>2</sub>@FeOOH@Fe, with core-shell structures were obtained. The overall process of SiO<sub>2</sub>@FeOOH@Fe synthesis is shown in Fig. 1. Meanwhile, in order to study the effect of FeOOH on degradation efficiency, the SiO<sub>2</sub>@Fe was also prepared as well as SiO<sub>2</sub>@FeOOH@Fe but used SiO<sub>2</sub> as a carrier.

To compare the degradation efficiency of the new synthetic material and NZVI on BDE209, NZVI was synthesized according to previous literature [37]. Briefly, EtOH (30 vol%) was used to prepare 0.2 g L<sup>-1</sup> FeSO<sub>4</sub>·7H<sub>2</sub>O and 0.16 g L<sup>-1</sup> NaBH<sub>4</sub>. Under mechanical stirring, the NaBH<sub>4</sub> aqueous solution was added to FeSO<sub>4</sub>·7H<sub>2</sub>O; the resulting solution was continuously stirred until it turned black. The particles were separated by vacuum filtration, and separately rinsed thrice with deoxygenated water and EtOH. Finally, the particles were stored in a vacuum drying chamber until further use.

### 2.3. Characterization

TEM (TECNAI 10, PHILIPS, The Netherlands) was used to observe the size and morphology of the particles. Thermogravimetric and differential thermal simultaneous analyses (STA 409 PC/4/H, NETZSCH, Germany) were performed in the atmosphere from room temperature to 800 °C at a heating rate of 10 °C min<sup>-1</sup>. Particle surface elemental analysis was performed using XPS (ESCALAB 250, Thermo-VG Scientific, USA) with light as the mono Al K $\alpha$  (energy: 1486.6 eV, scan mode: CAE, full spectrum scan: pass energy of 150 eV, narrow spectrum scan: pass energy of 20 eV). The crystalline phase of different particles was determined using an X-ray diffractometer (Y-2000, Dandong, China) with a Cu K $\alpha$  radiation. The accelerating voltage and applied current were 30 kV and 20 mA, respectively. FT-IR spectra of SiO<sub>2</sub>@FeOOH and SiO<sub>2</sub> was recorded on a IR-prespige-21 spectrometer (Shimadzu, Japan). The specific surface area and porosity were measured by an ASAP2020M instrument (Micromeritics Instrument Corp, USA). Fe content was measured by an inductively coupled plasma (ICP) optical emission spectrometer (IRIS Intrepid II XSP, Thermo Elemental Company, USA).



**Fig. 1.** (a) Schematic illustration of immobilization of nano zero-valent iron nanoparticles on mesoporous silica microspheres, (b) photograph of  $\text{SiO}_2$ ,  $\text{SiO}_2@ \text{FeO}$ , and  $\text{SiO}_2@ \text{FeO}@ \text{Fe}$ .

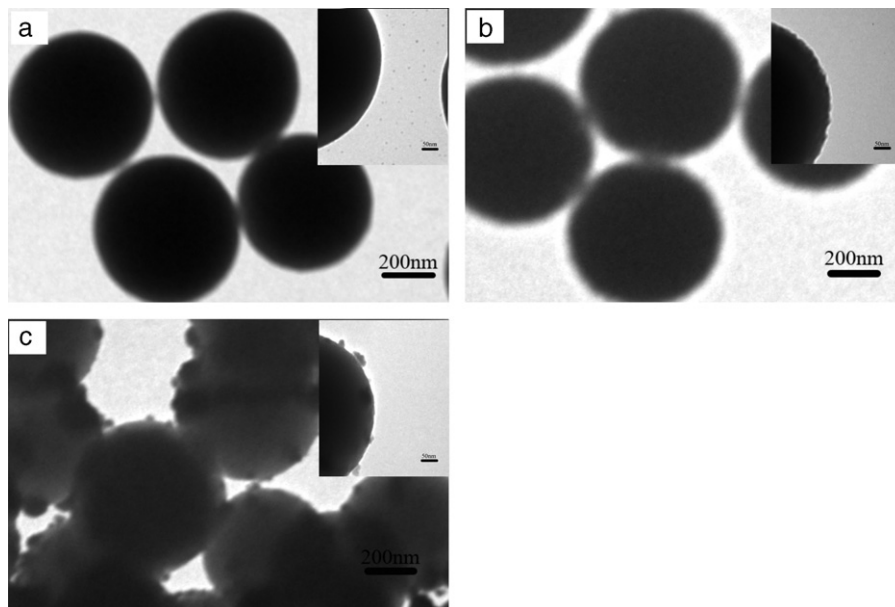
## 2.4. Degradation of BDE 209 by $\text{SiO}_2@ \text{FeO}@ \text{Fe}$

### 2.4.1. Preparation of the BDE209 solution

BDE209 with high hydrophobicity is difficult to dissolve in water [38,39]. To verify the feasibility of using the new method to remove the BDE209 from a solution, many researchers choose organic solvents (e.g., tetrahydrofuran (THF) [40], methane [41], and acetonitrile [42]) in their experiments. Therefore, the stock solution ( $100 \text{ mg L}^{-1}$ ) of BDE209 was made using pure THF as the solvent. A BDE209-simulated solution with the desired concentration was prepared by spiking a known volume of the stock solution with a certain proportion of the THF/water (v/v) solution, such as 4/6, 8/2, 7/3 and pure THF.

### 2.4.2. Batch experimental procedure

Batch degradation tests were performed in a 10 mL glass tube with a plug. For each batch, certain particles were added to the tubes, after each 10 mL of the simulated BDE209 solution at a certain concentration were added. The tubes were placed in an oscillator with a speed of 200 rpm at room temperature and then plugged with polytetrafluoroethylene. One of the tubes was removed at each interval, and the solution was extracted with a syringe. The extracted solution was filtered through a  $0.45 \mu\text{m}$  filtration membrane, and the BDE209 concentration was tested by liquid chromatography. Parallel experiments were followed the same procedures above. Control experiments were also performed without particles.



**Fig. 2.** TEM images of (a)  $\text{SiO}_2$ , (b)  $\text{SiO}_2@ \text{FeOOH}$ , and (c)  $\text{SiO}_2@ \text{FeOOH}@ \text{Fe}$ . The insets show the blowup TEM images of one sphere surface.

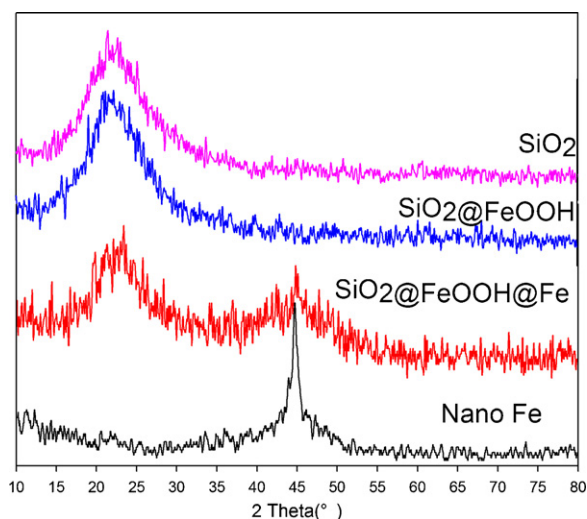


Fig. 3. XRD pattern of  $\text{SiO}_2$ ,  $\text{SiO}_2@FeOOH$ ,  $\text{SiO}_2@FeOOH@Fe$  and NZVI.

### 2.5. Analysis methods

The concentration of BDE209 in these samples was determined by HPLC (Shimadzu, LC10A HPLC) with a UV detector (SPD-10AV) at 240 nm. A Dikma C18 column (250 mm  $\times$  4.6 mm) was used. The mobile phase was 100% methanol delivered at a rate of 1.2 mL  $\text{min}^{-1}$ . Each sample size was 20  $\mu\text{L}$ . Quantification was done with a calibration curve of the BDE209 standard.

## 3. Results and discussion

### 3.1. Characterization of synthetic material

TEM photographs for  $\text{SiO}_2$ ,  $\text{SiO}_2@FeOOH$ , and  $\text{SiO}_2@FeOOH@Fe$  are shown in Fig. 2. Fig. 2a shows that the mesoporous silica microspheres synthesized by dodecylamine and tetraethoxysilane were uniform in size with an average diameter of 450 nm. The edges of the silica microspheres were observed under higher magnification, and their surface was observed to be smooth in the absence of modification (Fig. 2a).

When coated with an FeOOH layer, the sizes of the particles did not significantly change, but their surface became rough with an abundance of embossed points (Fig. 2b) and more  $-\text{OH}$  was brought by FeOOH layer may enhance the electronegativity of mesoporous silica microspheres. In the solution system containing 30% ethanol (the solution used in the synthetic process), the zeta electric potential of the mesoporous silica microsphere of unmodified FeOOH was  $-15.78$  mV, while the one of modified FeOOH was  $-25.78$  mV. Due to the zeta electric potential of nano zero-valence iron particle of  $+5.21$  mV, the silica microsphere of modified FeOOH can provide a better electric charge environment of the surface to realize a better combination with the particle.

Fig. 2c shows mesoporous silica microspheres loaded with NZVI. A number of small particles within 100 nm were attached to the surface of the microspheres; these particles were determined to be NZVI. Most of NZVI existed in the exterior of mesoporous silica microspheres because the size of nano zero-valent iron and formed protruding points, which can facilitate contact and reaction with pollutants.

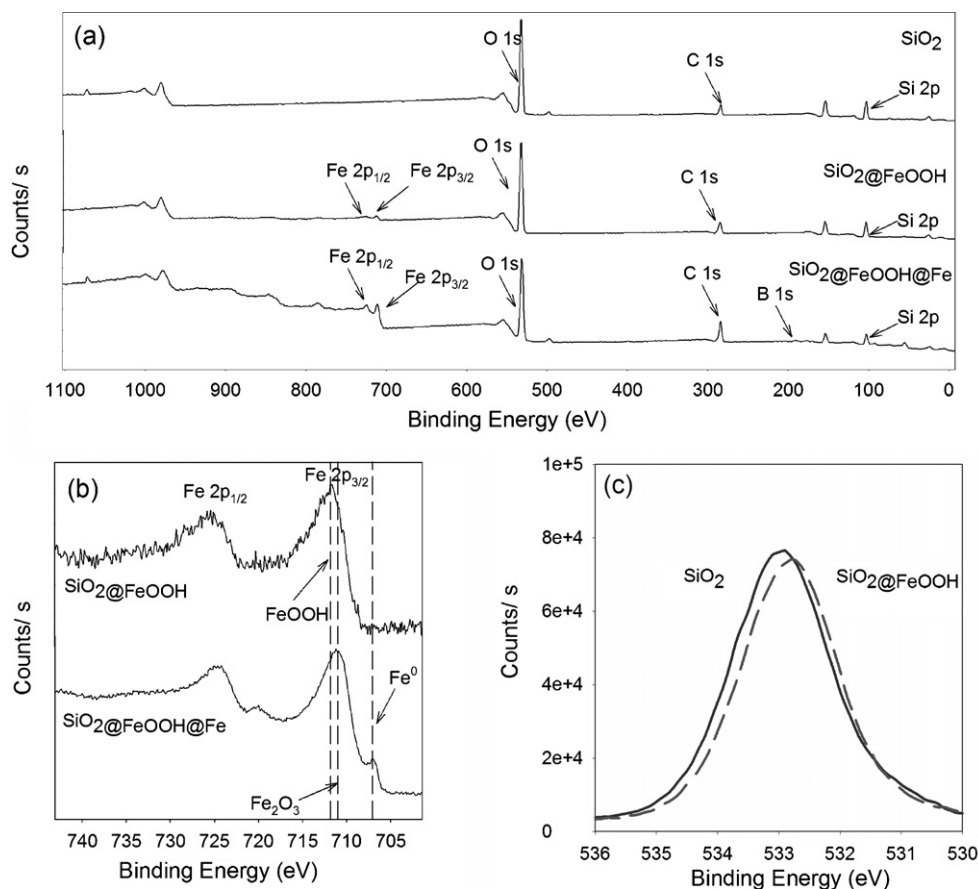


Fig. 4. (a) XPS spectra of  $\text{SiO}_2$ ,  $\text{SiO}_2@FeOOH$ , and  $\text{SiO}_2@FeOOH@Fe$ , (b) XPS spectrum for the narrow scan of Fe 2p on the surface of  $\text{SiO}_2@FeOOH$  and  $\text{SiO}_2@FeOOH@Fe$ , (c) XPS spectrum for the narrow scan of O 1s on the surface of  $\text{SiO}_2$ ,  $\text{SiO}_2@FeOOH$ .

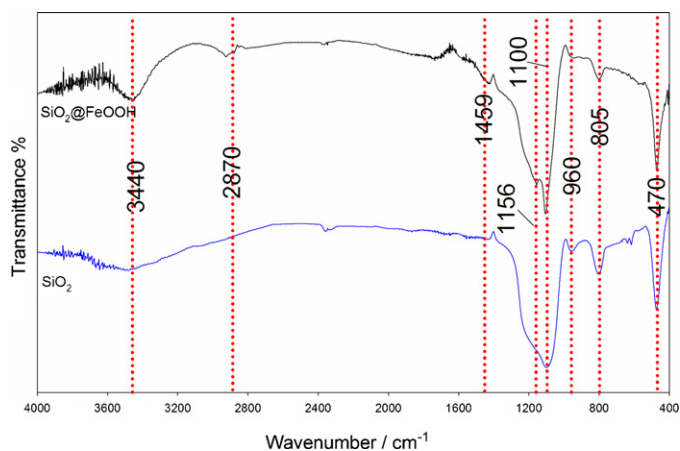


Fig. 5. FT-IR of  $\text{SiO}_2$  and  $\text{SiO}_2@FeOOH$ .

The XRD pattern of the synthesized particles is shown in Fig. 3. From the Fig. 3, except the characteristic diffraction peaks of silica and composite silica at  $28^\circ$  and peaks of zero-valent iron at  $44^\circ$ , we can see that no other peak like oxide iron appeared in the XRD graph. This may be caused by the rare contents of iron oxide. Therefore, XPS was further introduced to study the surface chemical compositions. Results from XPS analysis are shown in Fig. 4. From the full spectrum scan (Fig. 4a), significant Fe 2p binding energy peaks are found on the surface of  $\text{SiO}_2@FeOOH$  and  $\text{SiO}_2@FeOOH@Fe$  compared with  $\text{SiO}_2$  (Si 2p, C 1s, and O 1s). B 1s binding energy peak on the surface of  $\text{SiO}_2@FeOOH@Fe$  was produced due to the reduction between  $\text{NaBH}_4$  and the Fe ions. Fig. 4b shows Fe 2p of  $\text{SiO}_2@FeOOH$  and  $\text{SiO}_2@FeOOH@Fe$ , where the 711.5 eV binding energy of Fe 2p in  $\text{SiO}_2@FeOOH$  corresponded to that of FeOOH [43,44], indicating that the Fe in the second layer existed in the form of FeOOH. In the spectrogram of Fe 2p of  $\text{SiO}_2@FeOOH@Fe$ , binding energies of 706.9 and 710.8 eV corresponded to the ZVI and Fe oxidation states ( $\text{Fe}_2\text{O}_3$ ), respectively. This indicates that the NZVI particles are covered with an oxide film. This film could have been generated during the preparation process. The characteristic peak of O in the Si–O bond at 1s (Fig. 3c) shifted from 532.8 ( $\text{SiO}_2$  curve) to 531.1 eV ( $\text{SiO}_2@FeOOH$ ), indicating a shift to lower energy because Si–O–H turned to Si–O–C after PEG was grafted by  $\text{SiO}_2$  to the surface of the spheres. C has a larger electro-negativity than H (H: 220, C: 245), thus the characteristic peak shifted to lower energy levels. However, due to the electron donating effect of the Si–O-linked alkyl, the surface charge density of the Si and O atoms increased, which enhanced the shielding effects on the 2p electron of the Si atom and the 1s electron of the O atom. Consequently, the binding energies of the 2p electron of the Si atom and the 1s electron of the O atom were weakened, proving that PEG chains were incorporated into  $\text{SiO}_2$  [45]. In order to further confirm the PEG was successfully grafted to  $\text{SiO}_2$ , infrared spectroscopy of  $\text{SiO}_2$  and  $\text{SiO}_2@FeOOH$  has been carried out. As shown in the Fig. 5, there was a wide and large absorption band within the wave number of  $3440\text{ cm}^{-1}$ , which mainly caused by the adsorbed water on the surface and the stretching vibration of O–H in the Si–OH. Meanwhile, the absorption peak at  $805\text{ cm}^{-1}$  and  $470\text{ cm}^{-1}$  was caused by the symmetric stretching vibration of Si–O–Si. In addition, the absorption peak at  $960\text{ cm}^{-1}$  was caused by the bending vibration of Si–OH on the surface of silica microsphere. While as for  $\text{SiO}_2@FeOOH$ , except the characterization band of  $\text{SiO}_2$ , there are still the C–H absorption peaks at  $2870\text{ cm}^{-1}$ , as well as the C–H absorption peak  $1459\text{ cm}^{-1}$ . The C–O–Si stretching vibration peak also appeared at the  $1156\text{ cm}^{-1}$ . Combined with the TGA results we discussed in the manuscript, these all showed that the PEG was successfully grafted to  $\text{SiO}_2$ .

Table 1

Specific surface area and porosimetry of different particles.

	BET ( $\text{m}^2\text{ g}^{-1}$ )	Average pore diameter (nm)	Particle size (nm)
NZVI	35.6962	11.548	50–80
$\text{SiO}_2$	543.3220	2.1098	400–500
$\text{SiO}_2@FeOOH$	130.9155	2.1627	400–500
$\text{SiO}_2@FeOOH@Fe$	383.4766	2.1704	400–500

Fig. 6 shows the simultaneous thermal analysis of  $\text{SiO}_2$ ,  $\text{SiO}_2@FeOOH$ , and  $\text{SiO}_2@FeOOH@Fe$ . In the differential scanning calorimetry curves for these three materials, endothermic peaks at 85.1, 83.6, and 83.9  $^\circ\text{C}$ , representing the evaporation of water, corresponded to weight loss rates of 8.34%, 7.36%, and 6.31%, respectively. The quality of the elemental silica microspheres did not vary significantly as the temperature increased. However, several evident changes for  $\text{SiO}_2@FeOOH$  and  $\text{SiO}_2@FeOOH@Fe$  were observed. The qualities of these compounds significantly changed when the temperature increased from 160 to near 340  $^\circ\text{C}$ , mainly due to the dehydration of FeOOH to  $\text{Fe}_2\text{O}_3$  and carbonization of PEG. The exothermic peaks that appeared at 277.6 and 310.7  $^\circ\text{C}$  were caused by the combustion of PEG. The nanoscale particles on the surface appeared to play a hindering role, and the burning temperature of PEG for  $\text{SiO}_2@FeOOH@Fe$  was higher than that for  $\text{SiO}_2@FeOOH$ . The appearance of the combustion peak proves that PEG was grafted onto the microspheres. The quality of the  $\text{SiO}_2@FeOOH$  materials continued to decline, probably due to OH<sup>−</sup> losses in the  $\text{Fe}_2\text{O}_3$  structure when FeOOH was completely converted to  $\text{Fe}_2\text{O}_3$ . The weight of  $\text{SiO}_2@FeOOH@Fe$  started to increase between 400 and 500  $^\circ\text{C}$ , and an apparent exothermic peak was generated at 439.9  $^\circ\text{C}$ . These may have been caused by the conversion of NZVI to  $\text{Fe}_2\text{O}_3$  by combustion. The results here are consistent with those obtained for the thermoanalysis of NZVI by Ponder et al. [46]. Because surface layer of nano zero-valent iron was formed during the preparation. And that iron oxide layer cover on the surface of nano zero-valent iron effectively delayed oxidation of inner zero-valent iron during the simultaneous thermal analysis.

Fig. 7 shows the nitrogen adsorption–desorption isotherms of  $\text{SiO}_2$ ,  $\text{SiO}_2@FeOOH$  and  $\text{SiO}_2@FeOOH@Fe$ . The nitrogen adsorption isotherm is similar to that of Miyake et al. [35] and Araki et al. [47], which is type IV nitrogen adsorption–desorption isotherms according to the IUPAC classification and showed features of mesoporous materials. The specific surface area of silica oxide was  $543.322\text{ m}^2\text{ g}^{-1}$ , as measured by the nitrogen adsorption–desorption method, indicating that the material has a large specific surface area. The average pore diameter was 2.11 nm, indicating that the microsphere has a mesoporous structure. This also indicated by the small-angle XRD pattern of the prepared  $\text{SiO}_2$  microspheres. As shown in Fig. S1 (see Supplementary data), a single broad XRD peak was observed at around  $2.8\text{--}2.2^\circ$  means that some order pore structure exists in the sample. Moreover, combined with the HRTEM image of mesoporous silica microspheres (Fig. S2, see Supplementary data) and some reports [47], the sphere we synthesized contained pore and the nanostructure may be a wormhole-like pore structure. However, the specific surface area decreased after the spheres were covered with a FeOOH film (loading weight ratio of the Fe particle is 1.8% as measured by ICP). The specific surface area decreased to about  $130.916\text{ m}^2\text{ g}^{-1}$ . After loading the NZVI, the specific surface area of the spheres became  $383.477\text{ m}^2\text{ g}^{-1}$ . Although this specific surface area was lower than that of pure silica oxides, it was still higher than that of NZVI ( $35\text{ m}^2\text{ g}^{-1}$ ). The ICP results indicate that the mass of Fe account of 18.01% of those of the microsphere composites. The BET specific surface area and average pore diameter are summarized in Table 1.

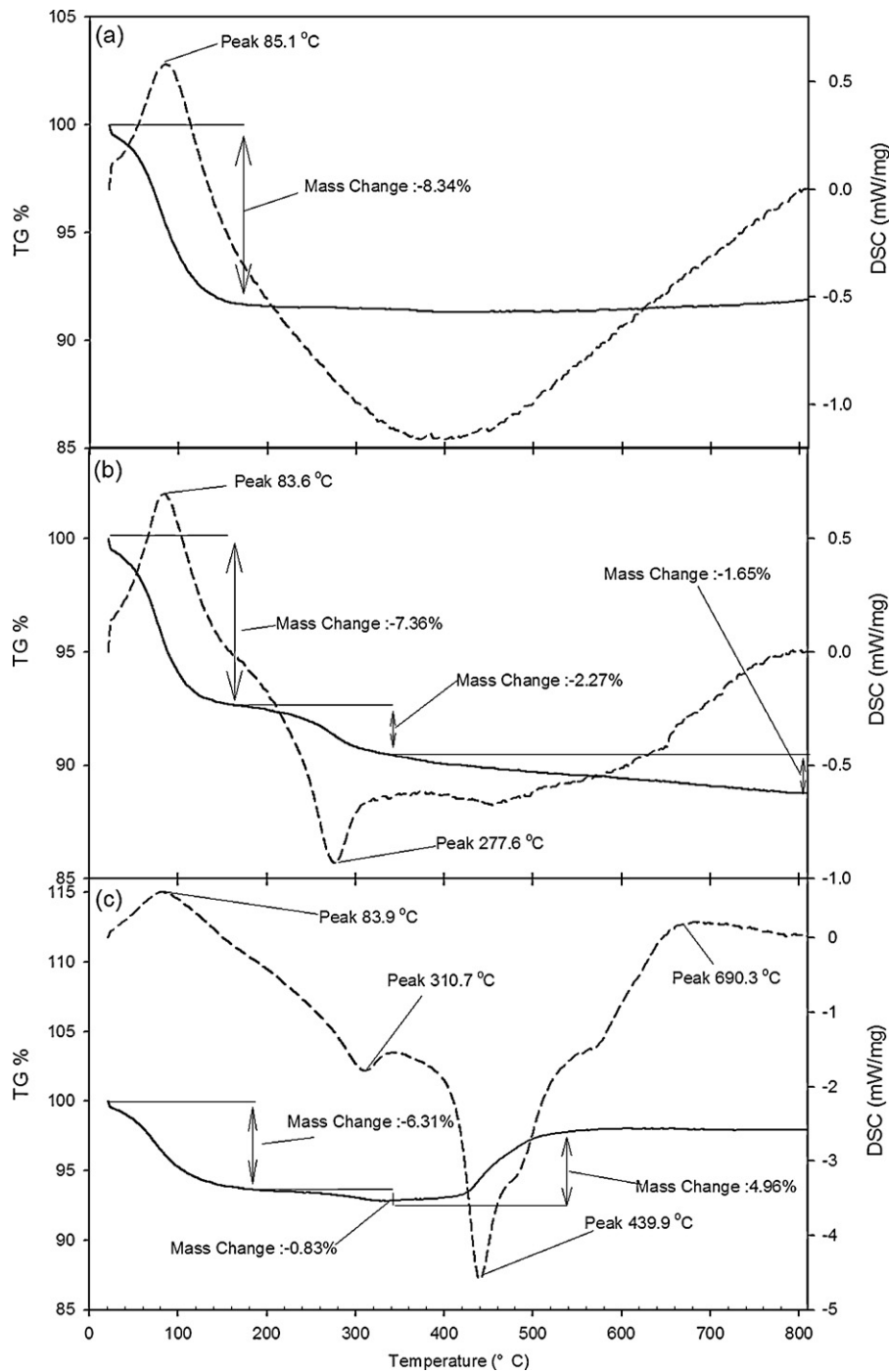


Fig. 6. Thermoanalysis of (a) SiO<sub>2</sub>, (b) SiO<sub>2</sub>@FeOOH, and (c) SiO<sub>2</sub>@FeOOH@Fe.

### 3.2. The effect of FeOOH on degradation

As shown in the Fig. 8, it is clearly showed that the degradation effectively of BDE209 by SiO<sub>2</sub>@FeOOH@Fe was faster than SiO<sub>2</sub>@Fe. At the end of reaction, near 100% of BDE209 have been removed by SiO<sub>2</sub>@FeOOH@Fe, but 65.48% for the SiO<sub>2</sub>@Fe. The reason can be the existence of FeOOH layer in SiO<sub>2</sub>@FeOOH@Fe provided more adsorption sites to facilitate the absorption of pollutant. So the silica microsphere, having modified FeOOH, has better removal efficiency than unmodified one during the reaction process.

### 3.3. Comparison of the degradation efficiency by different particles

Fig. 9a shows the degradation efficiency of BDE209 over time by different particles. Under the same quality of NZVI, 39.36% of the BDE209 was removed by the nano Fe during 8 h of oscillation, whereas 94.15% of the BDE209 was removed in 8 h by SiO<sub>2</sub>@FeOOH@Fe. This shows that SiO<sub>2</sub>@FeOOH@Fe presents superior degradation efficiency compared with nano Fe. Previous reports showed that organic halogenated contaminants are

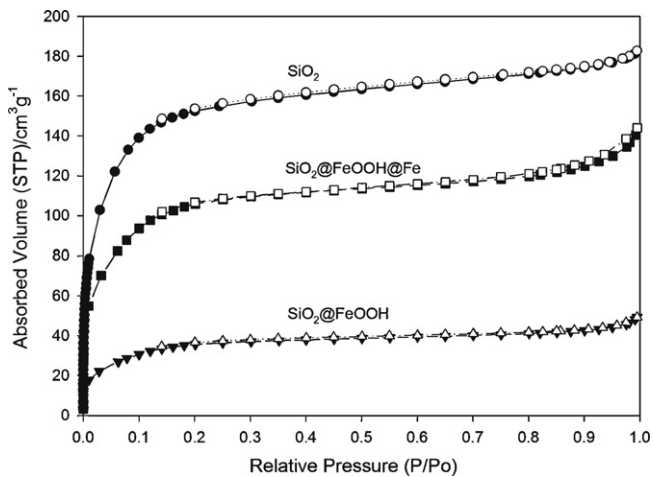


Fig. 7. Nitrogen adsorption/desorption isotherms of  $\text{SiO}_2$ ,  $\text{SiO}_2\text{@FeOOH}$ , and  $\text{SiO}_2\text{@FeOOH@Fe}$ .

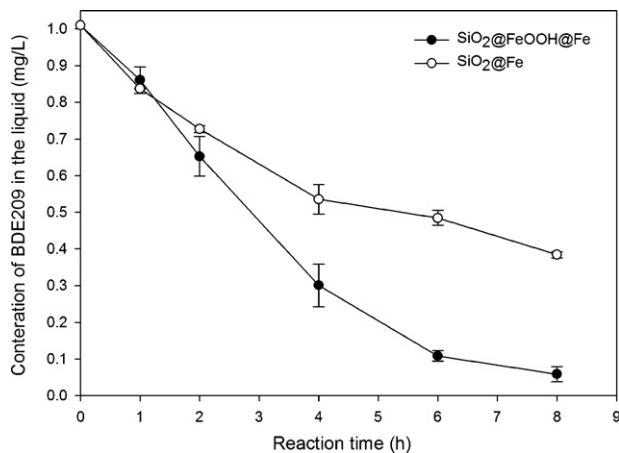


Fig. 8. Effect of FeOOH on the debromination efficiency. (Fe loading of  $\text{SiO}_2\text{@FeOOH@Fe}$  and  $\text{SiO}_2\text{@Fe}$  were  $3.96 \text{ g L}^{-1}$ ; initial concentration of BDE209,  $1 \text{ mg L}^{-1}$ ; reaction time, 8 h; temperature,  $28 \pm 2 \text{ }^\circ\text{C}$ ; and pH 6.09.)

removed by ZVI through a hydrogenation and debromination process. This process can be expressed by the following Eqs. (1)–(3) [48–50]: ( $X = \text{Cl}, \text{Br}$ ):

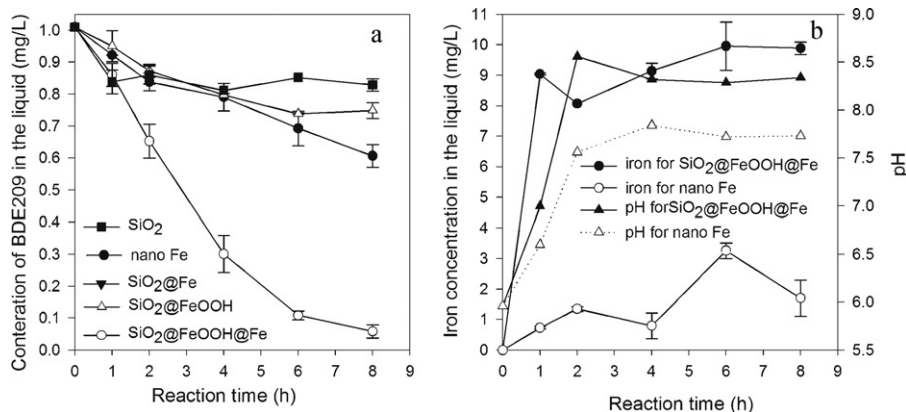
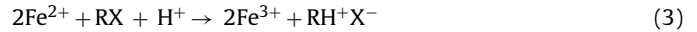
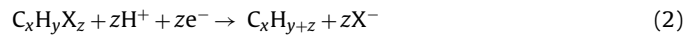


Fig. 9. (a) Comparison of BDE209 degradation by NZVI,  $\text{SiO}_2$ ,  $\text{SiO}_2\text{@FeOOH}$ , and  $\text{SiO}_2\text{@FeOOH@Fe}$ . (b) Concentration of iron ion and pH value of NZVI and  $\text{SiO}_2\text{@FeOOH@Fe}$ . (NZVI addition,  $4 \text{ g L}^{-1}$ ;  $\text{SiO}_2$ ,  $\text{SiO}_2\text{@FeOOH}$ , and  $\text{SiO}_2\text{@FeOOH@Fe}$  addition,  $22 \text{ g L}^{-1}$ . Fe loading of  $\text{SiO}_2\text{@FeOOH@Fe}$  was 18.01 wt%; initial concentration of BDE209,  $1 \text{ mg L}^{-1}$ ; reaction time, 8 h; temperature,  $28 \pm 2 \text{ }^\circ\text{C}$ ; and pH 6.09.)

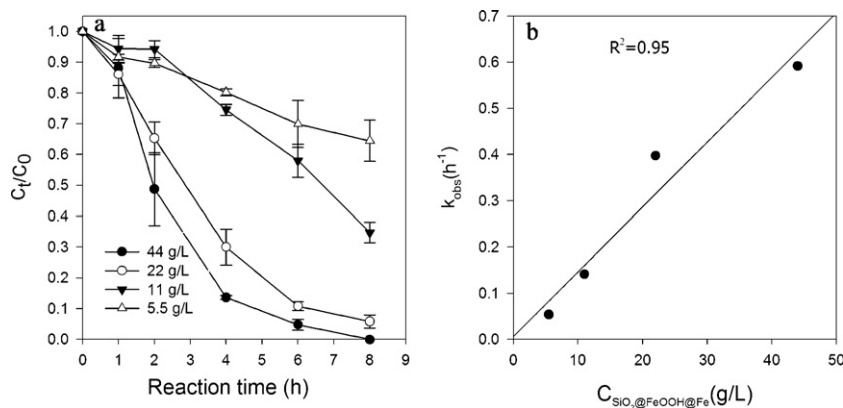


From these equations, H ions in the solution will be consumed in the reaction, resulting in increases in pH and Fe ions until equilibrium is reached. At equilibrium, the Fe ions will react with  $\text{OH}^-$  and then begin to precipitate. Therefore, the concentration of Fe ions and pH can approximately reflect the reaction rate during its early stages. The concentrations of Fe ions and pH changed over time during the reactions of nanoscale Fe and  $\text{SiO}_2\text{@FeOOH@Fe}$  (Fig. 9b). Comparing the reaction systems, the concentration of Fe ions and pH of  $\text{SiO}_2\text{@FeOOH@Fe}$  were significantly higher than those of the nanoscale Fe, indicating that  $\text{SiO}_2\text{@FeOOH@Fe}$  was more reactive. In addition, the kinetics of BDE209 removal by  $\text{SiO}_2\text{@FeOOH@Fe}$  and NZVI can be calculated by the equation, which is the expression of Langmuir–Hinshelwood kinetics model and also called the pseudo first-order model [51]:

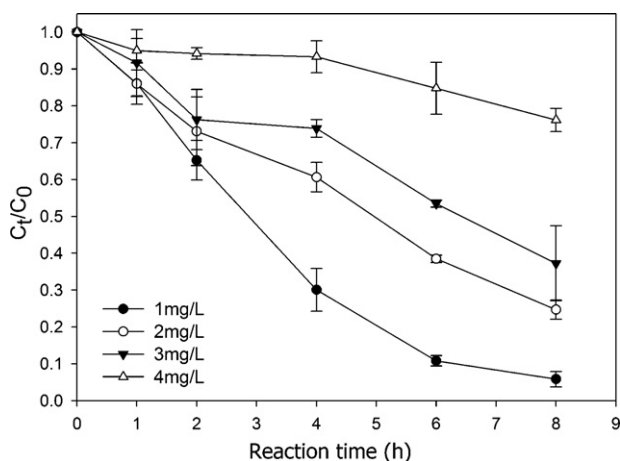
$$\ln \frac{c_t}{c_0} = -k_{\text{obs}}t \quad (4)$$

where  $c_t$  is the concentration of BDE209 at selected times ( $\text{mg L}^{-1}$ );  $c_0$  is the initial BDE209 concentration ( $\text{mg L}^{-1}$ );  $k_{\text{obs}}$  is the observed rate constant ( $\text{h}^{-1}$ ); and  $t$  is time (h). The observed reaction rate constant ( $k_{\text{obs}}$ ) values were calculated by the method of linear regression. The rate constants of the nanoscale Fe and  $\text{SiO}_2\text{@FeOOH@Fe}$  obtained from Eq. (4) were  $0.0569 \text{ h}^{-1}$  and  $0.3974 \text{ h}^{-1}$ , respectively. The rate constant of  $\text{SiO}_2\text{@FeOOH@Fe}$  was 6.9 times greater than that of NZVI. The degradation process of NZVI is a surface reaction. In addition to the good dispersion of  $\text{SiO}_2$  in water,  $\text{SiO}_2\text{@FeOOH@Fe}$  is more likely than NZVI to be exposed to BDE209 in the absence of a carrier and a stabilizer. This difference in dispersibility can be shown by the sedimentation experiments. As seen in Fig. S3 (see Supplementary data), most of the NZVI settled at the bottom of the colorimeter tube after 8 min, whereas  $\text{SiO}_2\text{@FeOOH@Fe}$  remained dispersed in the solution. This was because NZVI is prone to forming large particles by agglomeration, leading to a decline in its specific surface area and eventually reducing its dispersibility and reactivity. However, when NZVI is loaded onto the surface of  $\text{SiO}_2\text{@FeOOH}$ , the particles become more dispersed and difficult to coagulate due to the existence of a carrier, resulting in higher dispersibility and reactivity.

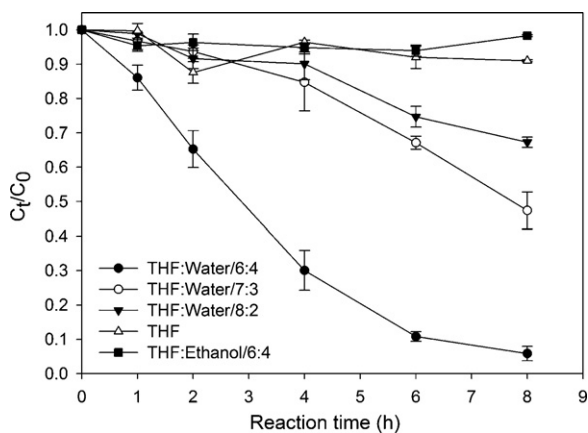
Both  $\text{SiO}_2\text{@FeOOH}$  and  $\text{SiO}_2$  have high specific surface areas. However, their removal efficiencies within 8 h were 25.12% and 17.08%, respectively. Although the results show that  $\text{SiO}_2$  covered with FeOOH layer can improve the removal efficiency of BDE209, both of them are not as efficient as the removal efficiencies of reactive nanoscale materials since  $\text{SiO}_2\text{@FeOOH}$  and  $\text{SiO}_2$  lack ability



**Fig. 10.** (a) Effect of SiO<sub>2</sub>@FeOOH@Fe addition on the degradation efficiency; (b) relationship of observed rate constant and the addition of SiO<sub>2</sub>@FeOOH@Fe. (Fe loading of SiO<sub>2</sub>@FeOOH@Fe was 18.01 wt%; initial concentration of BDE209, 1 mg L<sup>-1</sup>; reaction time, 8 h; temperature, 28 ± 2 °C; and pH 6.09.)



**Fig. 11.** Effect of the initial concentration on the degradation efficiency. (SiO<sub>2</sub>@FeOOH@Fe addition, 22 g L<sup>-1</sup>. Fe loading of SiO<sub>2</sub>@FeOOH@Fe was 18.01 wt%; reaction time, 8 h; temperature, 28 ± 2 °C; and pH 6.09.)



**Fig. 12.** Effect of solvent conditions on the BDE209 degradation efficiency. (SiO<sub>2</sub>@FeOOH@Fe addition, 22 g L<sup>-1</sup>, Fe loading of SiO<sub>2</sub>@FeOOH@Fe was 18.01 wt%; initial concentration of BDE209, 1 mg L<sup>-1</sup>; reaction time, 8 h; temperature, 28 ± 2 °C.)

of degradation. And these results also reflect that the adsorption capacity of SiO<sub>2</sub> to BDE209 is weak.

#### 3.4. Effect of SiO<sub>2</sub>@FeOOH@Fe particle addition

As shown in Fig. 10, the degradation efficiencies within 8 h are 100%, 94.15%, 65.24%, and 35.51% for 44, 22, 11 and

5.5 g L<sup>-1</sup> of SiO<sub>2</sub>@FeOOH@Fe particle addition, respectively. The degradation efficiency of BDE209 was improved with increasing SiO<sub>2</sub>@FeOOH@Fe dosages. The same pattern was reflected by the reaction rate constants obtained, which were 0.5917, 0.3974, 0.1413, and 0.0538 h<sup>-1</sup> for 44, 22, 11, and 5.5 g L<sup>-1</sup> of particle addition, respectively. When the data were plotted as the observed rate constant ( $k_{obs}$ ) against the mass loading of SiO<sub>2</sub>@FeOOH@Fe, a linear regression equation can be found in Fig. 10b, and the correlation coefficient ( $R^2$ ) of this line is 0.95, which clearly showed that the observed rate constant ( $k_{obs}$ ) is proportional to the mass loading of SiO<sub>2</sub>@FeOOH@Fe and  $k_{obs}$  can be improved by increasing the SiO<sub>2</sub>@FeOOH@Fe particle addition. This is because the degradation of BDE209 by SiO<sub>2</sub>@FeOOH@Fe can be described by the Langmuir–Hinshelwood mode, which suggests that the degradation process is occurred on the surface of the nanoscale metal and the surface reaction is the control step. Therefore, the surface area is an important factor for removing pollutants. The larger the surface area is, the larger the number of reaction sites, resulting in better adsorption and degradation capacity. Thus, increasing the dosage of nanoscale metals results in the provision of more reaction sites, leading to improved degradation efficiency [10,52].

#### 3.5. Effect of initial BDE209 concentration

Given that the concentration of SiO<sub>2</sub>@FeOOH@Fe was fixed at 22 g L<sup>-1</sup> at a steady reaction temperature of 28 ± 2 °C and that the initial concentrations of BDE209 were varied to 1, 2, 3, and 4 mg L<sup>-1</sup>, the relationship between the reaction time with different initial BDE209 concentrations and degradation efficiencies is illustrated in Fig. 11. After 8 h, the degradation rates were 94.15%, 75.3%, 62.73%, and 34.73% for the initial BDE209 concentrations of 1, 2, 3, and 4 mg L<sup>-1</sup>, respectively. As the initial concentration increased, the reaction rate constant gradually decreased from 0.3974 h<sup>-1</sup> at 1 mg L<sup>-1</sup> to 0.0492 h<sup>-1</sup> at 4 mg L<sup>-1</sup>. The degradation of BDE209 by SiO<sub>2</sub>@FeOOH@Fe is an interface reaction, the rate determining step is surface reaction. When kept the same mass loading of SiO<sub>2</sub>@FeOOH@Fe, with the more of pollutant concentration, the more degradation products of BDE209 on the surface of the material may occupy for reaction sites or compete with the BDE209 for reaction sites, thus affecting the degradation of BDE209 and causing the decline in the reaction rate of BDE209.

#### 3.6. Effect of solvent properties on degradation efficiency

To demonstrate the importance of protons in removing BDE209, degradation experiments were performed in different solvent systems. The influence of different solvent systems on BDE209



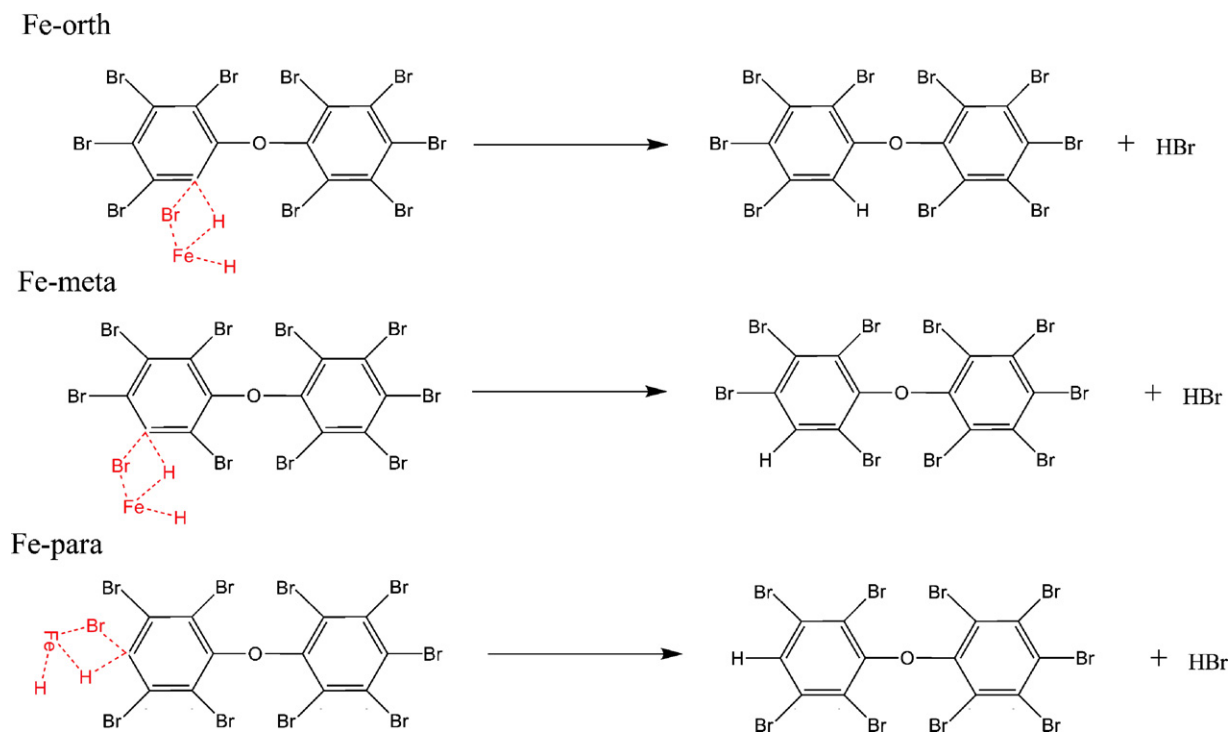
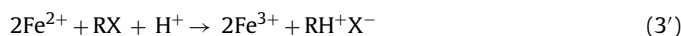
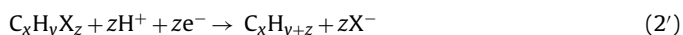


Fig. 13. Optimized transition state catalyzed by Fe.

degradation by  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$  is shown in Fig. 12. For pure THF or a mixture of THF and EtOH, no BDE209 was removed. The proportion of water in the solvent was one of the important factors that influenced debromination efficiency. When the water content in the solution was increased, BDE209 degradation was notably enhanced. After 8 h, the degradation efficiency of BDE209 was only 32.73% in the THF/water (8/2, v/v) solution; the degradation rate increased to 52.59% in the THF/water (7/3, v/v) solution and then to 94.15% in the THF/water (6/4, v/v) solution. Catalytic hydrogenation was proposed by Shih and Tai [11] and Li et al. [29] as the major pathway for the debromination process based on their experimental data. The base reaction of dehalogenation by NZVI could be depicted by Eqs. (1)–(3).



The reactions show that the presence of hydrogen ions in the solvent plays the most important role in the degradation of BDE209. The ionization constants ( $K_a$ ) of the different solvents used in the present paper followed this trend: water ( $K_a = 1 \times 10^{-14}$ ) > EtOH ( $K_a = 1 \times 10^{-30}$ ) > THF (aprotic solvent). This indicates that water can provide more hydrogen ions than other organic solvents for reduction. In an organic solvent system, the aprotic solvent is THF, and the system cannot provide hydrogen ions for the reaction. Although EtOH is a protic solvent like water, its ionization constants ( $K_a$ ) is  $10^{16}$  times smaller than that of water, so the solution could not provide enough protons for the reaction, resulting in slow or non-existent reactions.

Meanwhile, quantum chemistry was adopted to study the effect of different mixed solvent on the degradation of BDE209 by nano

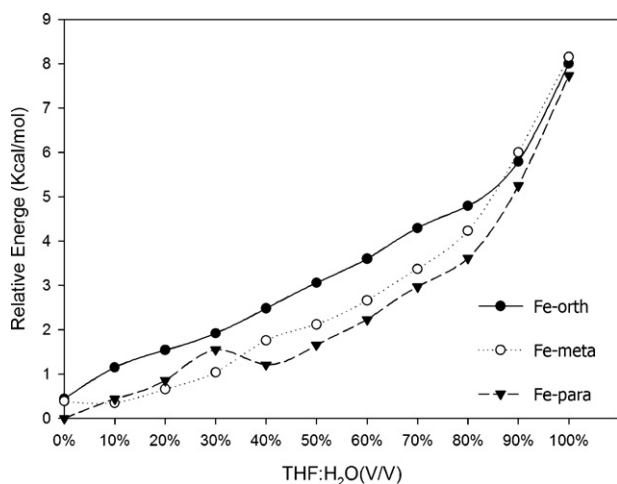


Fig. 14. Relative energies of optimized complex of metal Fe with BDE209 in different solvent.

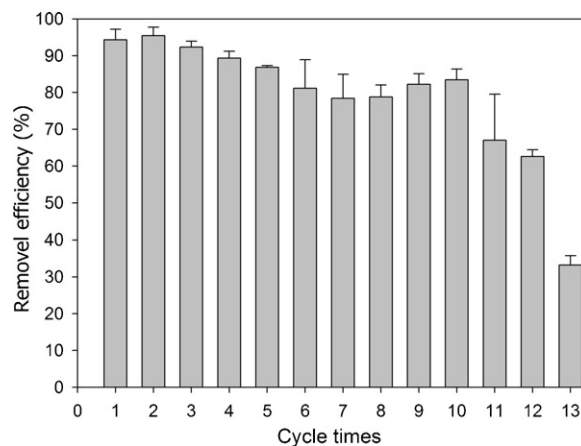


Fig. 15. Stability and durability of  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$  in BDE 209 degradation. ( $\text{SiO}_2@\text{FeOOH}@\text{Fe}$  addition,  $22 \text{ g L}^{-1}$ , Fe loading of  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$  was 18.01 wt%; initial concentration of BDE209,  $1 \text{ mg L}^{-1}$ ; reaction time, 8 h; temperature,  $28 \pm 2^\circ \text{C}$ ; pH 6.09.)

zero-valence iron further. All the calculations had been performed with the Gaussian 03 software package [53]. Molecular geometries were fully optimized at the Becke3LYP level of density functional theory [54–56]. What can be found is that besides providing hydrogen ion, the solvent has other impacts on degradation as follows. The first debromination of BDE209 by nano zero-valence iron shall form the following transition state (Fig. 13). This formation requires certain energy. The energy needed to form a transition state varied with different solvent and its water content. The following results are achieved by calculation. As we can see from the Fig. 14, with the decrease of water content, the energy needed increases constantly, which resulted in the slowdown of the reaction rate. This means that the reaction can be happened in the polar solvent condition more easier because the needed energies of forming transition state is less in the polar solvent. So the role of water is mainly not only to provide atomic hydrogen for the debromination, but also acts as a favorable composition of solvent for the debromination.

### 3.7. Stability and durability of $\text{SiO}_2/\text{FeOOH}/\text{Fe}$

To study the long-term degradation usability and stability of  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  for BDE209 degradation, 0.22 g of  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  and 10 mL of a  $1 \text{ mg L}^{-1}$  BDE209 solution were added to a 10 mL tube. The test tubes were sealed with a polytetrafluoroethylene plug, placed in an oscillator, and then agitated at a speed of 200 rpm. After one 8 h cycle, magnetic separation was used to separate the solution and particles, and all of the supernatant was removed, leaving the nanoparticles in the tube. Another 10 mL of the  $1 \text{ mg L}^{-1}$  BDE209 solution were added to the nanoparticles for one more cycle of degradation. The supernatant was filtered using a  $0.45 \mu\text{m}$  microporous membrane. The concentration of BDE209 was measured by HPLC, and the results are shown in Fig. 15.

From the first five cycles, the degradation rate of  $22 \text{ g L}^{-1}$   $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  for  $2 \text{ mg L}^{-1}$  BDE209 reached higher than 85% (Fig. 9). In the sixth cycle, the degradation rate dropped to 81.15%. In the seventh to tenth cycles, the degradation efficiency of  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  for BDE209 slightly declined, although it remained within 78% to 83%. Its performance began to decline significantly from the 11th cycle and even dropped to 33.21% in the 13th cycle. This may be due to the erosion of NZVI particles on the surface of  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  by water, leading to form oxidizing layer and a loss of reaction sites during continuous degradation. This can be determined by the XPS spectrums of  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  before and after reaction. As shown in the Fig. 16, it is clearly found that two peaks at the binding energies of 706.9 eV and 710.8 eV existed in the XPS spectra of Fe (2p) before reaction. Peak at 706.9 eV demonstrated the existence of NZVI, while broad peaks at 710.8 eV was attributed to iron oxides ( $\alpha\text{-Fe}_2\text{O}_3$ ). But for the XPS spectra of Fe (2p) after reaction, peak at 706.9 eV was disappeared and the 710.8 eV still exist. This means that the iron oxide was generated on the surface of particles during the reaction.

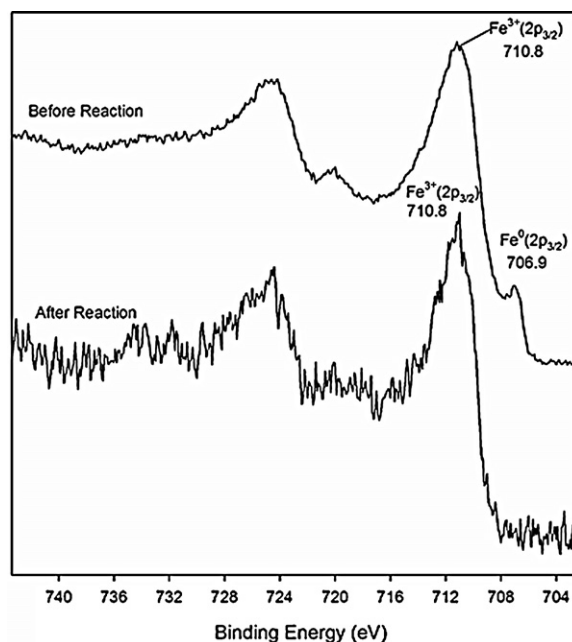


Fig. 16. XPS spectrum for the narrow scan of Fe 2p on the surface of  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$ . (a) Narrow scan of Fe 2p before reaction; (b) narrow scan of Fe 2p after reaction.

### 3.8. Anti-agglomeration and magnetic separation of $\text{SiO}_2/\text{FeOOH}/\text{Fe}$

To study agglomeration after prolonged storage, similar amounts of  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  and NZVI were placed inside a flask filled with EtOH. The flasks were then sealed and stored at room temperature. A month later, the morphologies of these two materials were obtained, as shown in Fig. 17. After one-month storage, NZVI apparently clustered and formed a block structure (Fig. 17a).  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  remained in almost the same condition (Fig. 17b), and the particles were dispersed evenly in the solution. This demonstrates the improved anti-agglomeration ability of  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$ , which is due to the presence of carriers in the particles. These carriers provide steric hindrance and weaken the agglomeration caused by the surface energy and magnetism between the nanoscale Fe particles.

$\text{SiO}_2/\text{FeOOH}/\text{Fe}$  has anti-glomeration properties and can be recovered by magnetism. Its magnetic hysteresis loop showed that its saturant magnetic induction ( $M_s$ ), coercive force, and magnetization ratio ( $M_r/M_s$ , where  $M_r$  is the magnetic remanence) were  $33.979 \text{ emu g}^{-1}$ ,  $235.97 \text{ G}$ , and  $0.18$ , respectively (Fig. 18a). This shows that  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  has ferromagnetic properties. When  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  particles were dispersed in an EtOH solution under an external magnetic field, the particles and solution were

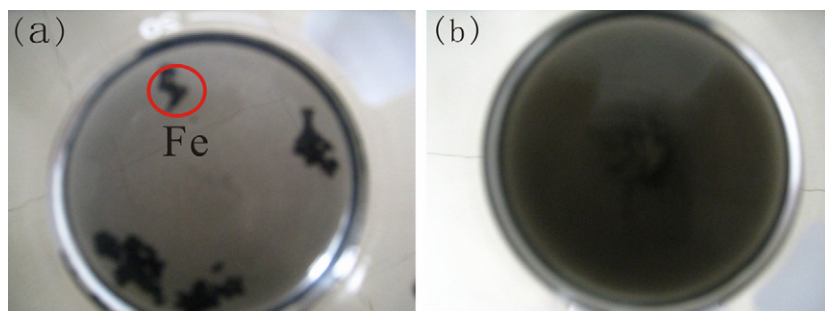
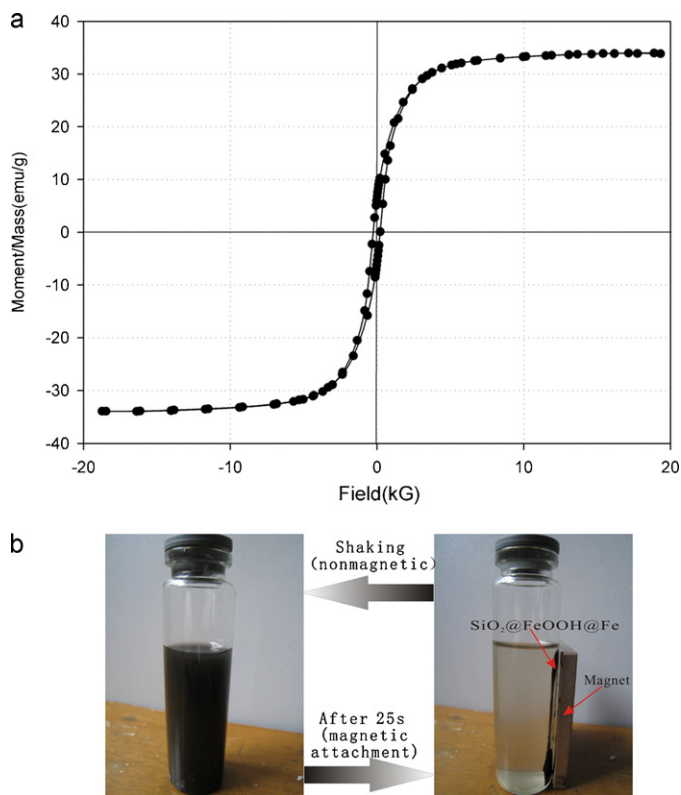


Fig. 17. Visual photos of (a) NZVI and (b)  $\text{SiO}_2/\text{FeOOH}/\text{Fe}$  after one month stored.



**Fig. 18.** (a) Magnetic hysteresis loop of  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$ . (b) The separation–dispersion process of  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$ .

fully separated after only 25 s (Fig. 18b). This shows the effective magnetic separation ability of  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$ .

#### 4. Conclusion

In the present study, we demonstrated a new approach for the immobilization of NZVI in mesoporous silica microspheres to enhance the dispersion of NZVI. Results from batch studies demonstrate that nanoscale  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$  is effective in removing BDE209 from a THF/water solution at ambient temperature and pressure. The degradation of BDE209 follows a pseudo-first order kinetics model and the degradation efficiency of BDE209 benefits from an increased amount of  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$ , resulting in a decrease in pollution levels. Through the reduction of BDE209 in different solvent condition and calculated the data by quantum chemistry, it strongly recommend that debromination is more effective in more water content due to hydrion was the driving forces of reaction and the energy needed to form transition state is less in polar solution. Comparing its degradation efficiency with that of NZVI and  $\text{SiO}_2@\text{Fe}$  under the same conditions, the degradation of BDE209 by  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$  is more efficient. In addition,  $\text{SiO}_2@\text{FeOOH}@\text{Fe}$  also shows potential practicality for its stable degradation within 10 cycles and better performance in agglomeration-resistance and separation. The results obtained in this study clearly show that immobilized Fe nanoparticles in mesoporous silica microspheres can be practically and efficiently used for removing BDE209.

#### Acknowledgments

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#### Appendix A. Supplementary data

Supplementary data associated with this article can be found, in the online version, at doi:10.1016/j.jhazmat.2011.07.024.

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